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# Decontamination Efficiency of Phenylethylene by an Activated Carbon-Based Adsorbent

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# ABSTRACT

A sudden leak of phenylethylene is an urgent issue for the surrounding environment. To mitigate its negative effect, the decontamination efficiency of phenylethylene on an activated carbon (AC)-based adsorbent was investigated. Factors such as the particle size and the temperature, that could affect the adsorption ratio, were explored. Meanwhile, the efficiency of AC, pretreated with different KMnO<sub>4</sub> and NaCIO concentrations, was examined. It was proven that the decontamination efficiency was higher for the 300-mesh AC compared to the 200-mesh AC. The introduction of the oxidizer, KMnO<sub>4</sub>, had a negative effect on phenylethylene adsorption. Nevertheless, the NaCIO-modified AC showed a positive influence on phenylethylene removal, while its decontamination gradually improved with the increase of the NaCIO concentration. It was also found that the adsorption rate of phenylethylene was ascended with the temperature rise. After 1 h of adsorption with AC heated to 200°C, no phenylethylene desorption was observed.

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# INTRODUCTION

Phenylethylene ( $C_8H_8$ ) is a typical volatile organic compound (VOC) (Ren et al. 2013), which is mephitic, toxic and flammable. Phenylethylene is an important organic chemical and is widely used in the production of synthetic resin, synthetic rubber, and ion-exchange resin. Its strong irritation and the narcotic effect would greatly harm people's respiratory tracts and eyes. In recent years, several phenylethylene leakage accidents have occurred in China (Yu 2012, Zhou et al. 2016), such as the phenylethylene leakage at the Yangtze River in 2001, the phenylethylene leakage due to tank car turnover in Lueyang City in 2010, and the phenylethylene spill at Jiangyin Section of the Yangtze River in 2011.

In case of emergency, the firefighters shall take simple and efficient measures to decontaminate hazardous chemicals quickly and conveniently. The decontamination materials should apply to the existing equipment and have a wide source, low cost, large output, and high adsorption efficiency (Jiang et al. 2017, Wang et al. 2016). Decontamination generally consists of chemical methods and physical methods. In particular, the physical methods include flushing, adsorption, evaporation, and reverse osmosis, while the chemical methods include neutralization, catalysis and oxidation (Li et al. 2014, Liu et al. 2010, Yao et al. 2016, Zhou et al. 2017).

Regarding the adsorption method, the decontamination is achieved by using a certain adsorbent to concentrate the

molecular pollutants on its surface or in the internal pores (Yu et al. 2019, Zhou et al. 2019, Zhou et al. 2015). The use of large Brunauer, Emmett and Teller (BET) and abundant micropores resulted in the adsorption capacity of AC up to 30-80 mg.g<sup>-1</sup> (Guo et al. 2010), employing mainly granular, powdered, and fibrous AC. In 2008 Pan et al. (2008) studied the adsorption of ammonia-modified AC and determined the porous structure and surface acid-base groups of several modified AC fibres, while the effect of the porous structure and the surface groups on the adsorption of phenylethylene was also discussed. Results showed that, after ammonia modification, the basic group content, the pore volume, and the BET features of the AC fibre surface increased, thus further improving the adsorption capacities of AC fibre on phenylethylene. In the study by Ren et al. (2013), AC and its modification were initially prepared from municipal sludge. The BET, acid-base group content, phenylethylene static adsorption, and desorption activation energy of AC were then compared before and after modification. It was demonstrated that the BET of sludge AC, modified by 0.1 M copper sulphate solution, was increased by 32% (705 m<sup>2</sup>.g<sup>-1</sup>) compared to the value prior to modification. The impregnation of the aluminium sulphate and copper sulphate solutions increased the surface acid group content of sludge AC, while the surface basic group content was reduced. Besides, the adsorption capacity of phenylethylene was increased more than two times compared to the precursor (211.4 and 178.8

mg.g<sup>-1</sup>, respectively). The adsorption penetration time for phenylethylene was increased from 2 to 10 min and the desorption activation energy was extended from 2.94 to >6.00 kJ.mol<sup>-1</sup>. Instead, Li et al. (2014) degraded phenylethylene by ozonation. Specifically, phenylethylene was effectively decontaminated by the ozone-coupled biological AC, whereas the decontamination rates of 1, 2, and 4 ppm phenylethylene were 100%, 60.6% and 57.9%, respectively.

The current study aimed to explore the decontamination behaviour of phenylethylene via AC in case of sudden leakage. The effect of particle size, thermal treatment, and oxidant modification on the phenylethylene adsorption on AC was investigated. Meanwhile, the second-order kinetic equation was used to illustrate the adsorption behaviour. The results of our investigation shed new light on the emergency disposal of sudden phenylethylene leakage.

## MATERIALS AND METHODS

#### **Reagents and Apparatus**

Phenylethylene was procured from Tianjin Tianli Chemical Reagent (China).  $KMnO_4$  and NaClO were obtained from Sinopharm Chemical Reagent (China). The abovementioned reagents were of analytical grade and dissolved in deionized water (18.2 M, Milli-Q, USA). AC was purchased from Jiangshan Lvyi Bamboo Charcoal (China) and was used after following purification process. After grinding and sieving, the AC was cleaned with deionized water before boiling. Afterwards, the solution was continuously stirred for 1 h and repeatedly flushed with deionized water to remove the surface impurity. Finally, the AC was dried for 12 h in a drying oven at 80°C. After being tested with the BET detector (ASAP 2460, Micromeritics, USA), the specific surface area of the

adsorbent reached 873.1 m<sup>2</sup>.g<sup>-1</sup> (Fig. 1).

Fig. 2 shows a self-made apparatus that was used during the current study. It mainly consisted of four parts, namely a decontamination chamber, a water treatment agent atomization injection system, a dry powder treatment agent injection system, and a foam injection system. The decontamination chamber consisted of a tank-8 (700 mm × 700 mm × 800 mm), an oil evaporating pan-21 (120 mm high), an air sac-7 (for balancing the chamber pressure during jet decontamination), a steam sampling tube-20, a filter-12, and a vapour concentration analyzer-13 (CEM200 Multi-Gas Emergency Detector, Beijing Taihua Hengyue Technology Development Co., Ltd.). The water treatment agent atomization injection system consisted of a sink-1, a liquid pump-2, a transfer tube-16, and a spray nozzle-3. The dry powder treatment agent injection system consisted of an air pump-4, a dry powder tank-5, a dry powder nozzle-6, a dry powder tube-18, and a compressed air tube-19. The foam injection system consisted of a foam concentrate tank-11, a foam concentrate tube-17, a foam pump-10, and a foam nozzle-9.

#### **Experimental Steps**

- 1. After treating the dry powder tank-5 with vacuum, it was added in the tank, and the pressure was adjusted to 8 bar. Then, the nozzle above the experimental tank was connected to the dry powder tank. Boiling water of 50 mm in height was added to the liquid tray-21 and 15 mL of phenylethylene were sprayed on the surface of the boiling water to accelerate the evaporation.
- The real-time monitoring was performed on the concentration of phenylethylene gas with the gas detector-13. When phenylethylene was substantially evaporated and



Fig. 1: Nitrogen adsorption-desorption isotherms and pore size distribution profiles (inset) of AC.

the concentration reached a constant level, the valve of the dry powder tank was opened to spray the dry powder.

3. The spraying was repeated 10 times, each of which lasted for about 2 s, and was completed in 3 min. The change in phenylethylene concentration was continuously monitored and when the concentration dropped to a constant level, the experiment was considered to be complete.

## **RESULTS AND DISCUSSION**

Effect of particle size: The 200 and 300-mesh AC are commonly used in the market and are applicable for firefighting equipment (Sun et al. 2017, Zhang et al. 2015). The 200 and 300-mesh AC powders were selected for this study as well to compare their effect on the phenylethylene decontamination. During the experiment, all the experimental conditions, including the amount of AC, the pressure of the dry powder tank, and the volatilization concentration of phenylethylene, were maintained constant. The real-time decontamination effect within five minutes is illustrated in Fig. 3.

The adsorption kinetics by the AC complied with the second-order kinetics, with insets showing the constants

( $\mathbb{R}^2 > 0.97$ ), indicating that the chemical adsorption is the rate-limiting step of the decontamination process (Liang et al. 2018, Yan et al. 2017). The decontamination rate of the 300-mesh AC was  $0.0127 \text{ h}^{-1}$ , i.e. about 1.25 times higher than the decontamination rate of the 200-mesh AC ( $0.0102 \text{ h}^{-1}$ ). Moreover, the 300-mesh AC had a lower phenylethylene residual rate (0.21 vs. 0.26), which indicated that its decontamination capability was greater than that of the 200-mesh AC. The 300-mesh AC had also smaller particle size, higher BET, and better hovering property, leading to improved phenylethylene elimination (Yu et al. 2017, Zhou et al. 2018).

**Effect of oxidant modification:** Fang et al. (2017) and Hu et al. (2017) documented that the oxidant impregnation could improve the adsorption capacity of the adsorbent. Based on these data, the 300-mesh AC was impregnated with a KMnO<sub>4</sub> solution and a NaClO solution and then used for the decontamination of phenylethylene. Fig. 4 presents the adsorption kinetics of phenylethylene using the AC impregnated with 1.5 g.L<sup>-1</sup> and 3.0 g.L<sup>-1</sup> of the KMnO<sub>4</sub> solution. The kinetics followed the second-order kinetic equation (R<sup>2</sup> >0.99), which demonstrated that the impregnation with KMnO<sub>4</sub> did not change the type of the phenylethylene adsorption kinetics. The decontamination process was still dominated by the



Fig. 2: Schematic diagram of the experiment.



Fig. 3: Decontamination kinetics of phenylethylene on AC at different mesh number. The inset is the corresponding parameters of the second-order model.

chemical adsorption. It was proven that the decontamination efficiency of phenylethylene was the same when using AC impregnated with 1.5 g.L<sup>-1</sup> of KMnO<sub>4</sub> (0.0117  $h^{-1}$ ) and 3.0 g.L<sup>-1</sup> of KMnO<sub>4</sub> (0.0116 h<sup>-1</sup>). Whereas, both of the impregnated AC manifested the inferior adsorption rate than their pristine predecessor  $(0.0127 h^{-1})$ , demonstrating that impregnation with KMnO<sub>4</sub> negatively affected the phenylethylene adsorption. The effect of the oxidation treatment on AC had two sides. Although the oxidant impregnation increased the number of the surface hydroxyl, carboxyl, and carbonyl groups, hence improving the decontamination efficiency, the oxidant could etch the surface and pore walls of AC and occupy partial pores. Such effects could concomitantly decrease the BET and the AC pore volume and reduce the adsorption sites (Fang et al. 2017, Zhou et al. 2016a, 2016b). In this study, KMnO<sub>4</sub> corroded the surface and pore walls of AC to such an extent that the negative impact predominated the positive effect.

According to previous reports, strong oxidants, such as nitric acid, easily damaged the pore walls, reduced the number of micropores, increased the number of mesopores and macropores, and reduced the BET, and the pore volume. Subsequently, they affected the adsorption efficiency (Gil & Grange 1997). Other studies (Wang et al. 2012) reported that the modification of AC with NaClO was relatively mild, indicating that the pore structure was slightly damaged, while the number of phenolic hydroxyl, carboxyl, ketonic, and ether surface oxygen-containing functional groups was increased (Rivera-Utrilla et al. 2011).

Hence, NaClO solutions with 5% effective chlorine and 10% effective chlorine were selected to treat AC, to carry out



Fig. 4: Decontamination kinetics of phenylethylene on AC after 1.5 and 3.0 g/L KMnO<sub>4</sub> immersion. The inset is the corresponding parameters of the second-order model.

the decontamination test. Fig. 5 describes that the adsorption rate of 5% NaClO impregnated AC was significantly elevated from 0.0127 to 0.0200  $h^{-1}$ , and further increased to 0.0217  $h^{-1}$  with the increase of NaClO concentration. This improvement substantiated that the impregnation with NaClO could gradually increase the active sites on the surface of AC and in turn the decontamination efficiency of phenylethylene.

Effect of thermal modification: Thermal treatment is an easily achievable physical method for controlling the surface functional groups and pore structures of AC (Fang et al. 2017). Herein, we investigated the decontamination efficiency of phenylethylene using AC treated at 100°C and 200°C and the obtained results are displayed in Fig. 6. The decontamination efficiency of phenylethylene after thermal modification was higher than that of pristine AC  $(0.0127 \text{ h}^{-1})$ , while their decontamination efficiency gradually elevated with rising temperature  $(0.0175-0.0190 h^{-1})$ . The adsorption capacity of the adsorbent for a specific adsorbate was mainly determined by physical properties such as BET, micropore volume, and pore size distribution, as well as its chemical properties such as the surface groups (Zhen et al. 2017, Zhen et al. 2016). The high-temperature activation improved the lattice structure of the AC, removed parts of impurities adsorbed on the surface and in the pores, and also increased the number of micropores or mesopores, thus increasing the BET of AC. Meanwhile, the high-temperature activation also oxidized some functional groups on the surface of AC, released a number of oxygen-containing functional groups, and enhanced the hydrogen bonding force, thus improving the adsorption efficiency (Fang et al. 2017).

Stability test: The adsorbed adsorbates may desorb over a



Fig. 5: Decontamination kinetics of phenylethylene on AC after 5% and 10% NaClO immersion. The inset is the corresponding parameters of the second-order model.



Fig. 6: Decontamination kinetics of phenylethylene on AC after 100 and 200°C heat treatment. The inset is the corresponding parameters of the second-order model.

long time (Zhou et al. 2016a, Zhou et al. 2017). The 200°C treated AC was selected to decontaminate phenylethylene and test its adsorption stability on AC. Fig. 7 illustrates the content of phenylethylene with the concomitant increase of the adsorption time, where an apparent decrease could be observed at a rudimentary stage spanning between 0-400 s. Subsequently, an equilibrium period was achieved. Specifically, the concentration of the phenylethylene gas in the decontamination chamber did not significantly rise within 1 h, indicating that the phenylethylene molecule was tightly adsorbed on AC and was hard to be desorbed.

#### CONCLUSIONS

Herein, the effect of the particle size, the oxidant modification, and the thermal treatment on the decontamination efficiency of phenylethylene was studied. The AC with a higher mesh number resulted in a greater decontamination efficiency. The modification of AC with  $KMnO_4$  decreased the efficiency, while it was increased with the NaClO modification and was further elevated with the increase of the NaClO concentration. Thermal treatment enhanced the adsorption rate of phenylethylene, which escalated with the temperature rise. No phenylethylene desorption was detected 1 h after the AC adsorption.

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Fig. 7: Adsorption stability of phenylethylene on AC.

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